

Hydrothermal Liquefaction of Digested Sewage Sludge to Produce Bio-Oil

Thermochemical conversion of digested sewage sludge in water or ethanol as an in-situ solvent system has been optimized at small and large scale

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AIM AND APPROACH

Sewage Sludge is a promising feedstock in several green chemistry processes due to its abundance. In this study, sewage sludge has undergone an anaerobic digestion at Bergen Biogas Facility.¹ The digested sewage sludge (DSS) (Figure 1, top) is converted in order to produce bio-oil (Figure 1, bottom), using hydrothermal liquefaction (HTL). Multivariate screening processes are performed to gain knowledge regarding which factors contribute to a higher oil yield and / or better specifications of the oil product itself. This is performed both in a reactor of 25 mL (Figure 2, top) and a larger one of 5.3 L (Figure 2, bottom), as previously reported with other feedstocks.²

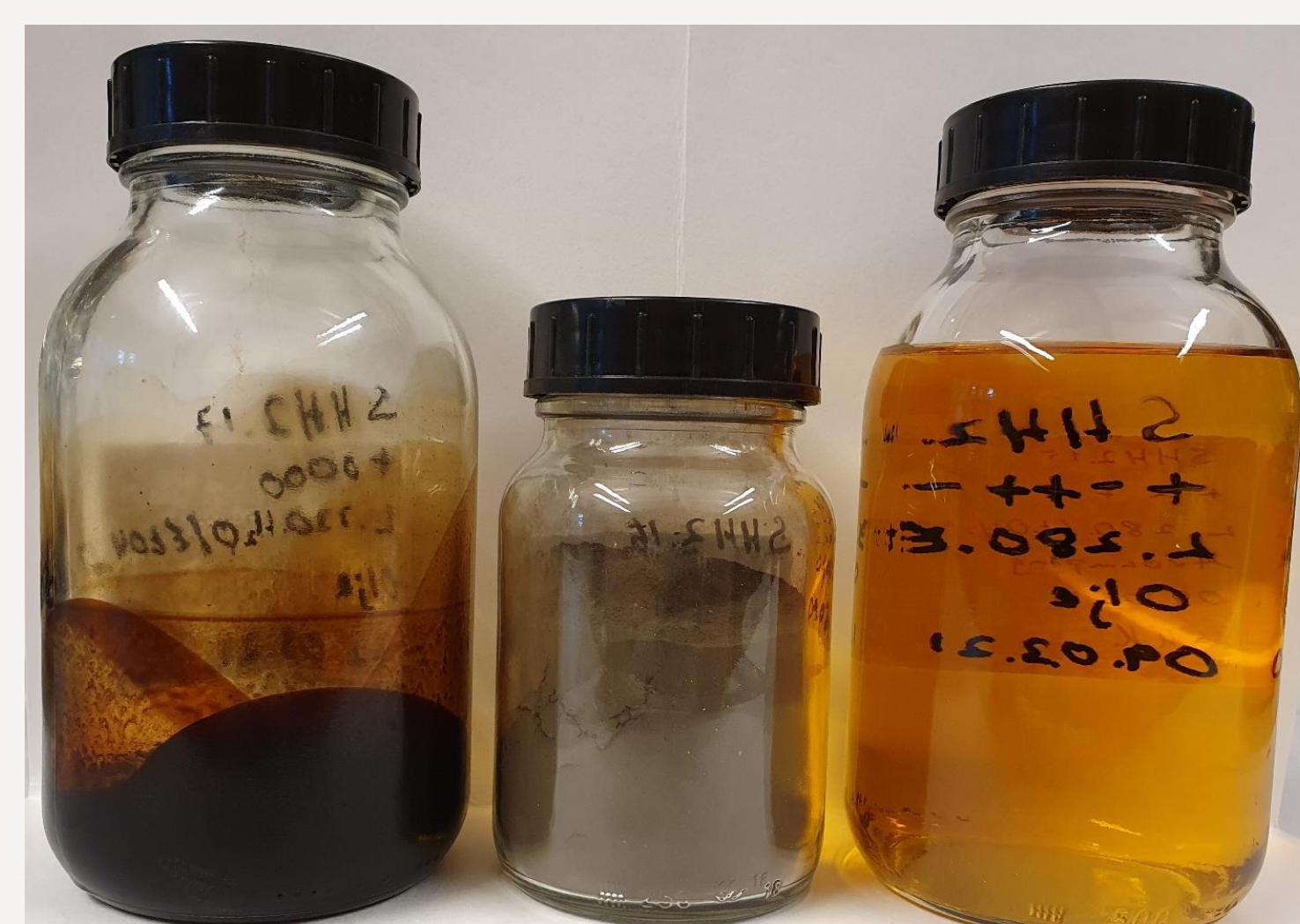


Figure 1: Top: Feedstock; Bottom: From left to right, bio-oil, coke, aqueous phase

EXPERIMENTAL

The process used is HTL in which the feedstock is heated and pressurized with an in-situ solvent system (water or ethanol) and formic acid (FA). Non-dried DSS, water or ethanol and FA is added to a reactor, which is then closed and heated to 280 – 380 °C for 2 – 6 hours. The oil is collected after cooldown, and separated from the gaseous-, solid- and aqueous product phases.

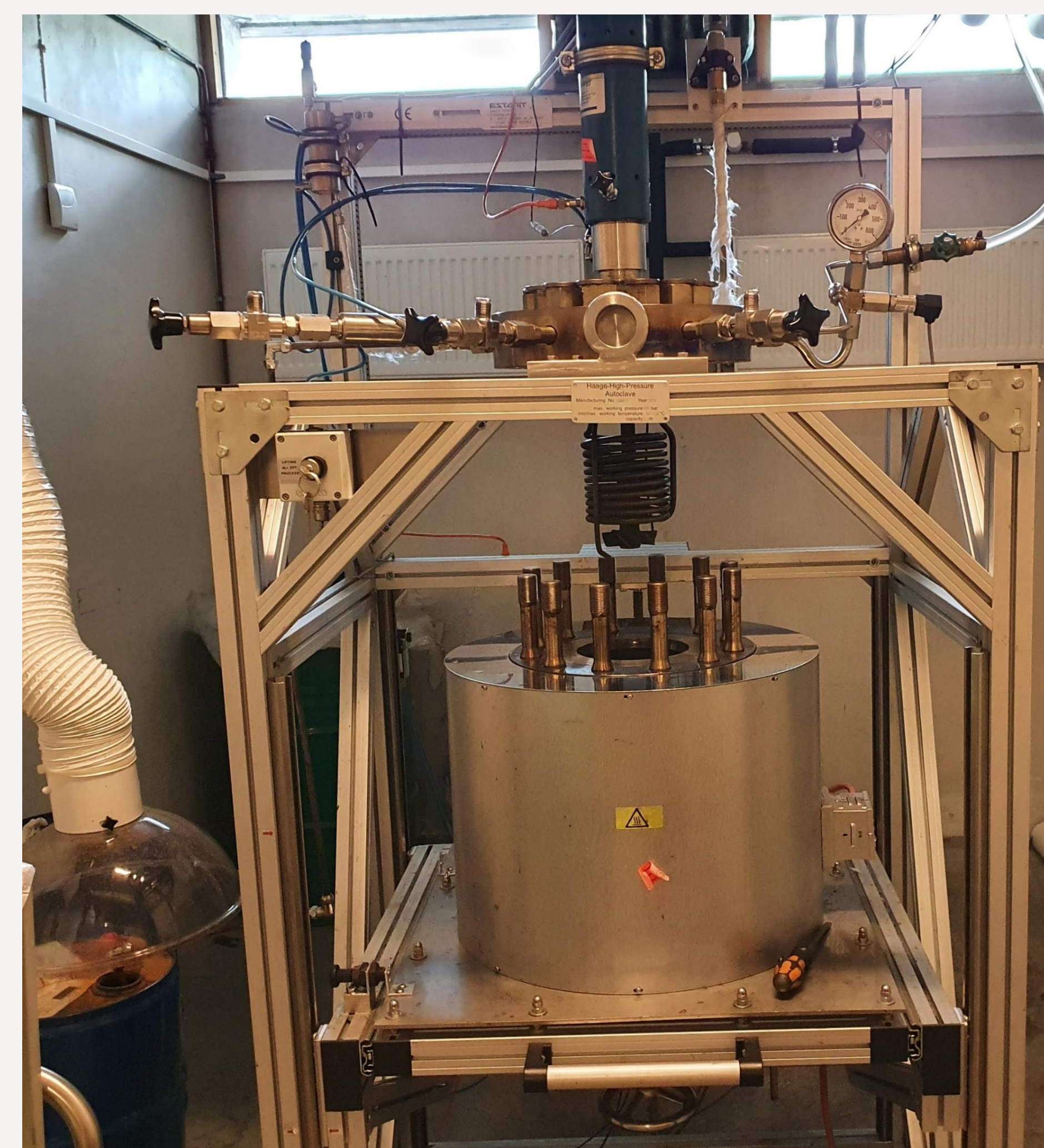


Figure 2: 25 mL reactor (top) and 5.3 L reactor (bottom)

RESULTS AND DISCUSSION

Oil Yields:

In the 25 mL reactor (Figure 2, top), the dry, ash free (*daf*) oil yield reached 29 – 73 %. The 5.3 L reactor (Figure 2, bottom) provided *daf* oil yields of 29 – 67 %. Table 1 shows the experimental conditions providing the highest oil yield for each reactor.

Table 1: Reaction conditions of the experiments based on fractional design, providing the highest yield in each reactor. + or – indicates whether this was the high or low variable setting:

	25 mL reactor	5.3 L reactor
m_{DSS} [g]	4	600
V_{FA} [mL]	1	150
t [h]	4	4
T [°C]	380 (+)	280 (-)
Solvent	EtOH	EtOH
$V_{solvent}$ [mL]	6 (+)	450 (-)
Stirring [rpm]	n.a.	1000 (+)

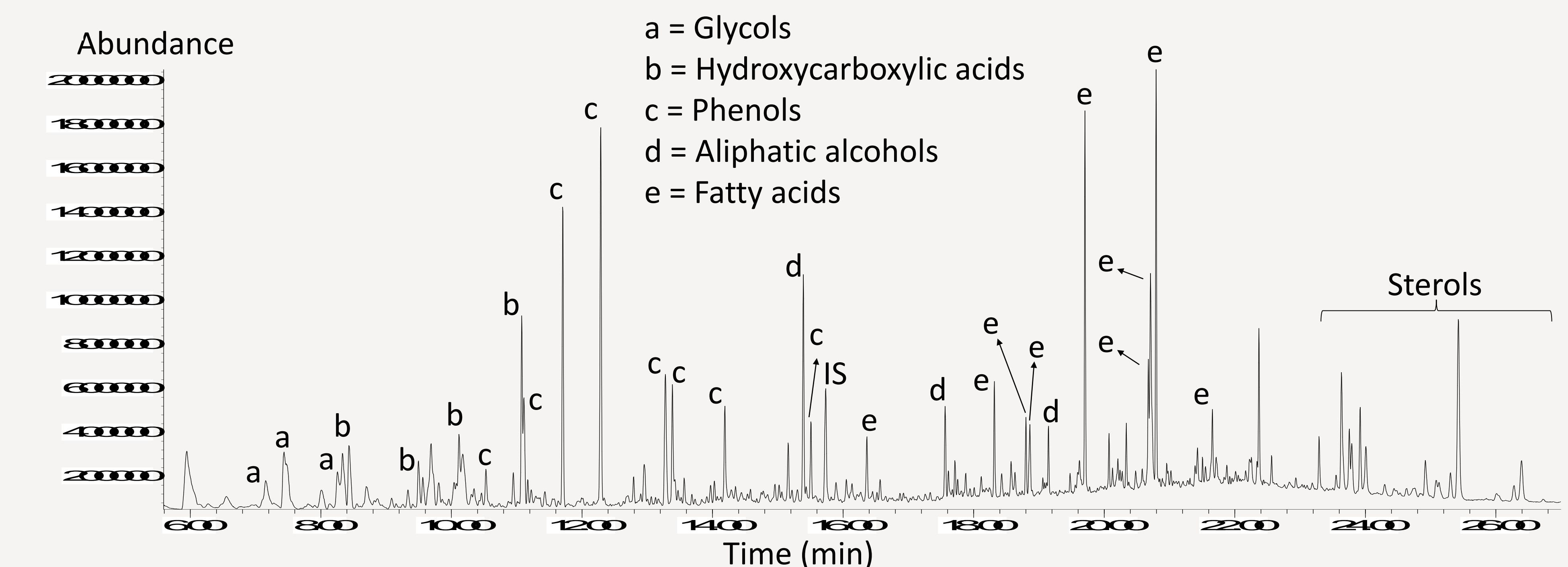


Figure 3: GC chromatogram showing a rough classification of compounds in the bio-oil

References

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